

## EXCESS AND DEVIATIONS PROPERTIES FOR THE BINARY SOLVENT MIXTURES OF TETRAHYDROFURFURYL ALCOHOL WITH SOME AROMATIC HYDROCARBONS AT 298.15K

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**ABSTRACT.** In this work, excess properties (e.g. excess molar volume ( $V^E$ ), excess viscosity ( $\eta^E$ ), excess Gibbs free energy of activation of viscos flow ( $\Delta G^{*E}$ ) and molar refraction changes ( $\Delta n_D$ ) of binary solvent mixtures of tetrahydrofurfuryl alcohol (THFA) with aromatic hydrocarbons (benzene, toluene and p-xylene) have been calculated. This was achieved by determining the physical properties including density  $\rho$ , viscosity  $\eta$  and refraction index  $n_D$  of liquid mixtures at 298.15K. Results of the excess parameters and deviation functions for the binary solvent mixtures at 298.15 K have been discussed by molecular interactions that occur in these mixtures. Generally, parameters showed negative values and have been found to fit well to Redlich-Kister equation which has been used to obtain the coefficients and evaluate the standard error.

**Keywords:** *Binary systems, Tetrahydrofurfuryl alcohol, Deviations and excess properties, Density, Viscosity.*

### INTRODUCTIONS

Interest in studying the theoretical and experimental properties of solvents mixtures has been significantly increased in the last two decades. The thermodynamic and transport information (e.g. fluids flow, heat and mass transfer) of mixtures systems are important in many chemical industries,

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solution theories and biological processes [1-4]. Moreover, for profound understanding the interaction properties between component molecules of liquid mixture, in terms of nature, strength of interaction and behavior of solution, the experimental excess properties are very important [5-8].

Tetrahydrofurfuryl alcohol (THFA), benzene, toluene and p-xylene are widely used in chemical industries. These solvents have been used in fuel, perfumes, cosmetics, lubricants, paints, dyes, printing ink, drugs, gums, resins, etc. [9,10]. The excess properties for these organic solvents are useful in investigating the molecular motion and packing, and interaction in their mixtures [11].

In this study, physical properties such as density, viscosity and refractive index were determined over a range of binary systems ((THFA+ Benzene), (THFA +Toluene) and (THFA+P-Xylene)) concentrations at 298.15K. Excess molar properties including  $V^E$ ,  $\eta^E$ ,  $\Delta G^{*E}$  and refractive index deviation were derived. Up to our knowledge, those binary solvent mixtures have not been studied for  $V^E$ ,  $\eta^E$ ,  $\Delta G^{*E}$ , and  $\Delta n_D$  at any temperature.

## RESULTS AND DISCUSSION

In this work the retrieved data from experimentally obtained density ( $\rho$ ) for binary systems (THFA + benzene, THFA + toluene and THFA + p-xylene) at 298.15 K were used to calculate  $V^E$  for binary solvent mixtures using following equation (1) [12]:

$$V^E = \frac{X_1 M_1 + X_2 M_2}{\rho_{12}} - \frac{X_1 M_1}{\rho_1} - \frac{X_2 M_2}{\rho_2} \quad (1)$$

where  $X_1$  and  $X_2$  are the mole fractions,  $M_1$  and  $M_2$  are the molar masses and  $\rho_1$ ,  $\rho_2$  are densities of solvents 1 and 2; while  $\rho_{12}$  is the density of the mixture. Values of  $V^E$  and  $\rho$  of the binary solvent systems at a range of mole fractions of THFA with benzene, toluene and p-xylene are presented in Table 1. Excess viscosities were obtained using equation (2) [13]:

$$\eta^E = \eta_{12} - (X_1 \eta_1 + X_2 \eta_2) \quad (2)$$

where  $\eta_1$  and  $\eta_2$  are viscosities of solvents 1 and 2, respectively,  $\eta_{12}$  is the viscosity of mixture. The results are listed in Table 1.

Equation 3 was used to calculate ( $\Delta G^{*E}$ ) [14]:

$$\Delta G^{*E} = RT[\ln(\eta_{12} V_{12}) - (X_1 \ln \eta_1 V_1) - (X_2 \ln \eta_2 V_2)] \quad (3)$$

where R is gases universal constant and T is the absolute temperature (K).  $V_1$ ,  $V_2$  are the molar volumes of solvents 1 and 2; while  $V_{12}$  is the molar volume for binary system. Table 1 shows the values of  $\Delta G^{*E}$  determined from equation 3.  $V_{12}$  has been obtained from the below equation:

$$V_{12} = (X_1M_1 + X_2M_2) / \rho_{12} \quad (4)$$

Molar refraction ( $n_D$ ) was calculated using the Lorentz-Lorenz equations (5,6, and 7) [15]

$$n_D = \left( \frac{n_{12}^2 - 1}{n_{12}^2 + 2} \right) \frac{X_1M_1 + X_2M_2}{\rho_{12}} \quad (5)$$

$$n_{D1} = \left( \frac{n_1^2 - 1}{n_1^2 + 2} \right) \frac{X_1M_1}{\rho_1} \quad (6)$$

$$n_{D2} = \left( \frac{n_2^2 - 1}{n_2^2 + 2} \right) \frac{X_2M_2}{\rho_2} \quad (7)$$

where  $n_{12}$  is the refractive index of the mixture; whereas  $n_1$  and  $n_2$  are the refractive index of solvent 1 and 2, respectively. The deviation from a molar fraction average of the molar refraction was computed according to the equation (8) [16,17]:

$$\Delta n_D = n_D - X_1n_{D1} - X_2n_{D2} \quad (8)$$

where  $\Delta n_D$  represents the deviation value from molar fraction. Table 1 lists experimental  $n_D$  and  $\Delta n_D$  for the binary solvent mixtures.

For binary solvent mixtures, the excess function was determined using Redlich-Kister model equation (9) [18]:

$$X^E = X_i X_j \sum_{K=0}^n A_K (X_i - X_j)^k \quad (9)$$

where  $X^E$  may represent  $V^E$ ,  $\Pi^E$ ,  $\Delta G^{*E}$  or  $\Delta n_D$ .  $X_i$  and  $X_j$  are the mole fractions of the components  $i$  and  $j$ , respectively.  $n$  is the degree of polynomial expansion and  $A_k$  denotes the polynomial coefficients. The equation (10) was used to calculate standard deviation ( $\sigma$ ) for the excess parameters [19]:

$$\sigma = \left[ \sum (X_{\text{exp}}^E - X_{\text{calc}}^E)^2 / (M - n) \right]^{1/2} \quad (10)$$

where  $M$  is the number of data points and  $n$  is the number of estimated parameters. The values of these coefficients and the standard deviation are given in Table 2.

For all the studied systems, the negative values of  $V^E$ ,  $\Pi^E$ ,  $\Delta G^{*E}$ ,  $\Delta n_D$  follow the order: Benzene > Toluene > p-xylene. Fig.1 shows the deviations in molar volume for all the systems (THFA+ benzene), (THFA+ toluene) and (THFA+ p-xylene). The obtained negative values of  $V^E$  can be attributed to the interactions of dipolar-induced forces between the benzene ring of the aromatic hydrocarbons and hydroxyl group (OH) or oxygen of the THFA, which results the formation of electron donor-acceptor complexes and the breaking of the self-associations existing in pure solvents [20,21].

**Table 1.** Experimentally obtained and calculated values of density, viscosity and refractive index,  $V^E$ ,  $\eta^E$ ,  $\Delta G^{*E}$ ,  $n_D$  and  $\Delta n_D$  for binary solvent mixtures of THFA+benzene, THFA+ toluene and THFA+ p-xylene at 298.15K.

<b>X<sub>1</sub> THFA + X<sub>2</sub> benzene at 298.15K</b>							
<b>X<sub>1</sub></b>	<b><math>\rho(\text{g.cm}^{-3})</math></b>	<b><math>V^E \text{ cm}^3\text{mol}^{-1}</math></b>	<b><math>\eta</math></b>	<b><math>\eta^E \text{ mpa.s}</math></b>	<b><math>\Delta G^{*E} (\text{J.mol}^{-1})</math></b>	<b><math>n_D</math></b>	<b><math>\Delta n_D</math></b>
0.0000	0.87372	0.00000	0.59951	0.00000	0.0000	1.4975	0.0000
0.0867	0.89294	-0.11763	0.65845	-0.08836	-218.2600	1.4882	-0.2377
0.2012	0.91623	-0.16936	0.81019	-0.12150	-299.6432	1.4754	-0.5832
0.3078	0.93673	-0.19441	0.99374	-0.14121	-348.0611	1.4664	-0.7895
0.3622	0.94663	-0.18579	1.10746	-0.14713	-362.5572	1.4636	-0.8175
0.5033	0.97132	-0.16189	1.48353	-0.15119	-372.4340	1.4581	-0.8077
0.5528	0.97965	-0.15214	1.65007	-0.14877	-366.4779	1.4571	-0.7589
0.6664	0.99804	-0.11675	2.13172	-0.13130	-323.4082	1.4552	-0.6238
0.8307	1.02332	-0.06816	3.09948	-0.10213	-251.8803	1.4545	-0.3136
0.9082	1.03474	-0.04150	3.77085	-0.06886	-169.9206	1.4536	-0.1879
1.0000	1.04761	0.00000	4.89883	0.00000	0.0000	1.4532	0.0000

<b>X<sub>1</sub> THFA + X<sub>2</sub> toluene at 298.15K</b>							
<b>X<sub>1</sub></b>	<b><math>\rho(\text{g.cm}^{-3})</math></b>	<b><math>V^E \text{ cm}^3\text{mol}^{-1}</math></b>	<b><math>\eta</math></b>	<b><math>\eta^E \text{ mpa.s}</math></b>	<b><math>\Delta G^{*E} (\text{J.mol}^{-1})</math></b>	<b><math>n_D</math></b>	<b><math>\Delta n_D</math></b>
0.0000	0.86224	0.00000	0.55464	0.00000	0.0000	1.4950	0.0000
0.0801	0.87733	-0.17517	0.55817	-0.16815	-416.0727	1.4855	-0.3714
0.2024	0.89945	-0.27578	0.67662	-0.24213	-598.5265	1.4750	-0.7081
0.3004	0.91712	-0.30678	0.82295	-0.25982	-641.8989	1.4670	-0.9415
0.3968	0.93436	-0.28668	1.01161	-0.26343	-650.4906	1.4624	-0.9856
0.5022	0.95335	-0.24312	1.27016	-0.26543	-655.2431	1.4581	-0.9821
0.5867	0.96872	-0.19668	1.55083	-0.24986	-616.8046	1.4562	-0.8887
0.7005	0.98983	-0.13909	2.08992	-0.19942	-492.1386	1.4553	-0.6653
0.7915	1.00704	-0.09509	2.64994	-0.16026	-395.4876	1.4547	-0.4714
0.8996	1.02791	-0.04847	3.57807	-0.09546	-235.6671	1.4539	-0.2334
1.0000	1.04761	0.00000	4.89883	0.00000	0.0000	1.4532	0.0000

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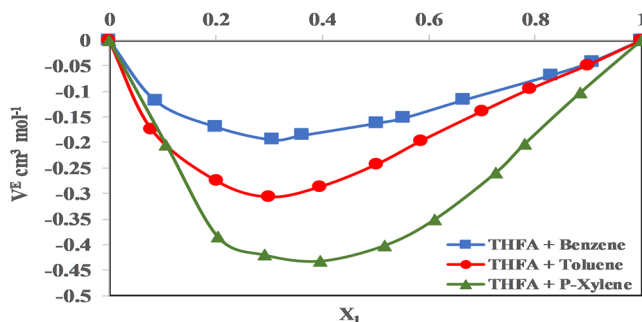
<b>X<sub>1</sub> THFA + X<sub>2</sub> p-xylene at 298.15K</b>							
<b>X<sub>1</sub></b>	<b>ρ(g.cm<sup>-3</sup>)</b>	<b>V<sup>E</sup> cm<sup>3</sup>.mol<sup>-1</sup></b>	<b>η</b>	<b>η<sup>E</sup> mpa.s</b>	<b>ΔG<sup>*E</sup> (J.mol<sup>-1</sup>)</b>	<b>n<sub>D</sub></b>	<b>Δn<sub>D</sub></b>
0.0000	0.85676	0.00000	0.61225	0.00000	0.0000	1.4945	0.0000
0.1074	0.87474	-0.20439	0.66272	-0.14414	-350.8699	1.4859	-0.5063
0.2045	0.89176	-0.38483	0.73091	-0.24813	-604.0360	1.4773	-0.9615
0.2921	0.90681	-0.42023	0.84477	-0.28553	-693.5423	1.4710	-1.2382
0.3968	0.92537	-0.43209	1.02825	-0.30671	-743.5405	1.4669	-1.3145
0.5168	0.94742	-0.40192	1.29614	-0.32474	-787.1356	1.4629	-1.2905
0.6108	0.96535	-0.35118	1.59703	-0.31146	-754.8408	1.4602	-1.1920
0.7255	0.98808	-0.25996	2.08926	-0.28134	-682.6599	1.4585	-0.9179
0.7811	0.99944	-0.20241	2.43108	-0.24543	-595.6440	1.4577	-0.7568
0.8856	1.02173	-0.10211	3.30304	-0.15625	-379.6321	1.4548	-0.4554
1.0000	1.04761	0.00000	4.89883	0.00000	0.0000	1.4532	0.0000

The results of deviations in viscosity ( $\eta^E$ ) for mixtures (THFA+ benzene), (THFA+ toluene) and (THFA+ p-xylene) are illustrated in Fig.2. Interaction between components molecules believed to be due dispersion or weak dipole-dipole forces [22]. Moreover, THFA contains molecules with high polarity while aromatic hydrocarbon are non-polar molecules having  $\pi$  - electrons on the ring. THFA molecules would induce a small dipole moment in the aromatic hydrocarbon molecule when mixed. A formation of a weak dipole-induced dipole interaction between the component molecules is also expected. In addition, donor acceptor interaction between  $\pi$ -electrons of benzene ring and oxygen of O-H group of THFA results in negative values of  $\eta^E$  [11].

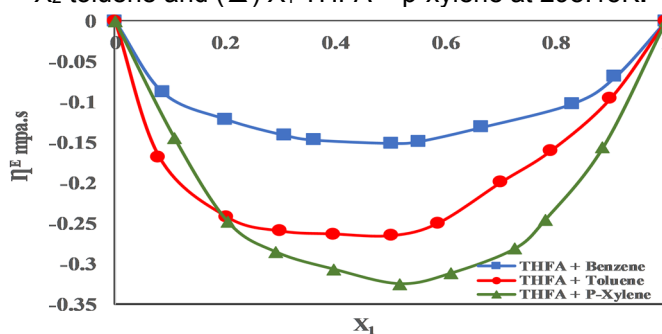
The plots of  $\Delta G^{*E}$  versus mole fractions ( $X_1$ ) at 298.15K for all the three binary systems (THFA + benzene, THFA + toluene and THFA + p-xylene) are presented in Fig.3. Values of  $\Delta G^{*E}$  were found to be negative for all the systems under study. The experimentally obtained negative  $\Delta G^{*E}$  and  $\eta^E$  values for all binary solvents mixtures show weak interactions between unlike molecules and indicate that flow is easier for the binary solvent mixtures when compared with that of pure solvents [23,24].

The deviations in  $\Delta n_D$  (molar refraction) was found to be negative for all binary systems over the composition range at investigated temperature (Fig.4). Generally, the negative values of  $\Delta n_D$  suggest weak interactions between the component molecules in the system [15]. For all binary solvent

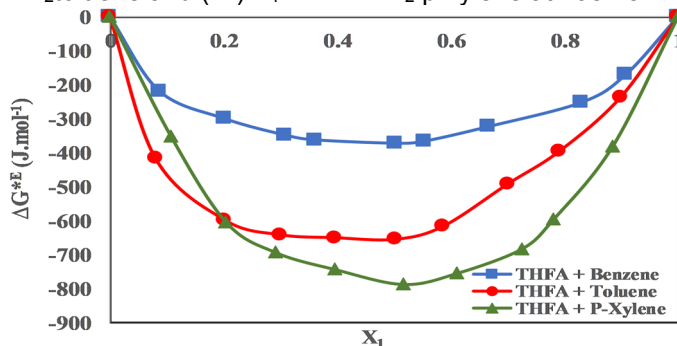
mixtures, the interactions of self-association are stronger than the specific interaction of unlike molecules, and the average interaction strength in mixture is weaker than that in the pure solvents.



**Figure 1.**  $V^E$  versus  $X_1$  for (■)  $X_1$  THFA +  $X_2$  benzene, (●)  $X_1$  THFA +  $X_2$  toluene and (▲)  $X_1$  THFA + p-xylene at 298.15K.

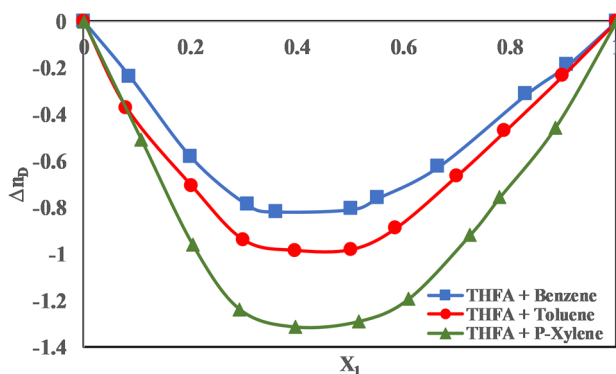


**Figure 2.**  $n^E$  versus  $X_1$  for (■)  $X_1$  THFA +  $X_2$  benzene, (●)  $X_1$  THFA +  $X_2$  toluene and (▲)  $X_1$  THFA +  $X_2$  p-xylene at 298.15K.



**Figure 3.**  $\Delta G^E$  versus  $X_1$  for (■)  $X_1$  THFA +  $X_2$  benzene, (●)  $X_1$  THFA +  $X_2$  toluene and (▲)  $X_1$  THFA +  $X_2$  p-xylene at 298.15K.

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**Figure 4.** Excess refractive index versus  $X_1$  for (■)  $X_1$  THFA +  $X_2$  benzene, (●)  $X_1$  THFA+ $X_2$  toluene and (▲)  $X_1$  THFA +  $X_2$  p-xylene at 298.15K.

**Table 2.** Polynomial coefficients ( $A_k$ ) and standard deviations ( $\sigma$ ) for binary solvent mixtures at 298.15K.

Function	System	$A_0$	$A_1$	$A_2$	$\sigma$
VE (cm <sup>3</sup> .mol <sup>-1</sup> )	THFA + Benzene	-0.64840	0.50722	-0.41527	0.00005
VE (cm <sup>3</sup> .mol <sup>-1</sup> )	THFA + Toluene	-0.96620	0.99681	-0.58565	0.02326
VE (cm <sup>3</sup> .mol <sup>-1</sup> )	THFA + P-Xylene	-1.65665	0.87340	-0.07943	0.02937
Function	System	$A_0$	$A_1$	$A_2$	$\sigma$
$\eta^E$ (mPa.s)	THFA + Benzene	-0.58614	0.07922	-0.45357	0.02414
$\eta^E$ (mPa.s)	THFA + Toluene	-1.02289	0.43810	-0.70071	0.03616
$\eta^E$ (mPa.s)	THFA + P-Xylene	-1.29209	0.00408	-0.47842	0.01902
Function	System	$A_0$	$A_1$	$A_2$	$\sigma$
$\Delta n_D$ (cm <sup>3</sup> .mol <sup>-1</sup> )	THFA + Benzene	-3.26617	1.03140	0.76222	0.03357
$\Delta n_D$ (cm <sup>3</sup> .mol <sup>-1</sup> )	THFA + Toluene	-3.89318	1.43064	0.49336	0.03873
$\Delta n_D$ (cm <sup>3</sup> .mol <sup>-1</sup> )	THFA + P-Xylene	-5.29561	1.18722	0.44150	0.03461
Function	System	$A_0$	$A_1$	$A_2$	$\sigma$
$\Delta G^{*E}$ (J.mol <sup>-1</sup> )	THFA + Benzene	-1443.65	196.1852	-1124.19	1.20126
$\Delta G^{*E}$ (J.mol <sup>-1</sup> )	THFA + Toluene	-2524.99	1086.265	-1737.40	1.80019
$\Delta G^{*E}$ (J.mol <sup>-1</sup> )	THFA + P-Xylene	-3131.71	15.89403	-1185.48	0.94697

## EXPERIMENTAL SECTION

### Chemicals

All solvents in this study (THFA, benzene, toluene and p-xylene) were purchased from Sigma-Aldrich and with purity of  $\geq 99\%$ , therefore, no further purifications were needed. Density  $\rho$ , viscosity  $\eta$  and refractive index  $n_D$  for solvents have been checked and examined against those listed in the literature (Table 3).

### Measurements

The densities ( $\rho$ ) were calculated (an average of three replicates) with accuracy of ( $\pm 0.00001 \text{ g.cm}^{-3}$ ) using a digital density meter (Anton paar, Model DMA 60/602). A controlled temperature suspended-level Ubbelohde viscometer was used for the measurement of viscosity ( $\eta$ ) under atmospheric pressure at  $298.15 \pm 0.01 \text{ K}$ .

The determinations of refractive indices for pure solvents and their binary solvent mixtures were performed using a digital Abbe refractometer (model: BOE 32400). For refractometer calibration, double distilled water used at  $298.15$ .

**Table 3.** Experimental and literature physical properties [density ( $\rho$ ), viscosity ( $\eta$ ) and refractive index ( $n_D$ )] of pure solvents at  $298.15 \text{ K}$ .

Compound	T/ K	$\rho \text{ (g.cm}^{-3}\text{)}$		$\eta \text{ mpa.s}$		$n_D$	
		Exp.	Lit. <sup>[ref]</sup>	Exp.	Lit. <sup>[ref]</sup>	Exp.	Lit. <sup>[ref]</sup>
THFA	298.15	1.04761	1.04761 <sup>[25]</sup>	4.89883	4.89883 <sup>[25]</sup>	1.4532	1.45322 <sup>[25]</sup>
Benzene	298.15	0.87372	0.87357 <sup>[26]</sup>	0.59951	0.6038 <sup>[26]</sup>	1.4975	1.4980 <sup>[27]</sup>
			0.87361 <sup>[27]</sup>		0.604 <sup>[28]</sup>		1.4971 <sup>[29]</sup>
			0.87360 <sup>[28]</sup>				
			0.87342 <sup>[29]</sup>				
Toluene	298.15	0.86224	0.86301 <sup>[26]</sup>	0.55464	0.5540 <sup>[26]</sup>	1.4950	1.4942 <sup>[27]</sup>
			0.86236 <sup>[27]</sup>		0.556 <sup>[28]</sup>		1.4931 <sup>[29]</sup>
			0.86220 <sup>[28]</sup>				
			0.86226 <sup>[29]</sup>				
p-xylene	298.15	0.85676	0.85670 <sup>[26]</sup>	0.61225	0.6078 <sup>[26]</sup>	1.4945	1.4933 <sup>[27]</sup>
			0.85682 <sup>[27]</sup>		0.611 <sup>[28]</sup>		1.4926 <sup>[29]</sup>
			0.85662 <sup>[28]</sup>				
			0.85670 <sup>[29]</sup>				

Exp.: experimental, Lit.: literature, [ref]: reference



## CONCLUSIONS

The values of  $\rho$ ,  $\eta$ , and  $n_D$  were calculated in binary solvent mixtures THFA with benzene, toluene and *p*-xylene over a range of mole fractions. Various excess properties like  $V^E$ ,  $\eta^E$ ,  $\Delta G^{*E}$ ,  $\Delta n_D$  were calculated from experimentally obtained thermodynamic values. For the binary solvent mixtures studied, benzene showed the most negative values of ( $V^E$ ,  $\eta^E$ ,  $\Delta G^{*E}$ ,  $\Delta n_D$ ) while *p*-xylene showed the least.

The experimental values of  $V^E$ ,  $\eta^E$ ,  $\Delta G^{*E}$ ,  $\Delta n_D$  were fitted well to Redlich-Kister equation. For all binary solvent mixtures, the interactions of self-association are stronger than the specific interaction of unlike molecules, while, the average interaction strength in mixture is weaker than that in the pure solvents.

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